

# The Sensitizing Effects of NO<sub>x</sub> on Methane Low-temperature Oxidation in a Jet Stirred Reactor

Lorena Marrodán<sup>1</sup>, Yu Song<sup>2</sup>, Nicolas Vin<sup>2</sup>, Olivier Herbinet<sup>2</sup>, Emmanuel Assaf<sup>3</sup>, Christa Fittschen<sup>3</sup>, Alessandro Stagni<sup>4</sup>, Tiziano Faravelli<sup>4</sup>, María U. Alzueta<sup>1</sup>, Frédérique Battin-Leclerc<sup>2</sup>

<sup>1</sup>Grupo de Procesos Termoquímicos (GPT)  
Instituto de Investigación en Ingeniería de Aragón (I3A)  
Universidad de Zaragoza, Mariano Esquillor s/n, 50018, Zaragoza, Spain.

Tel. +34-976762707, e-mail: [marrodan@unizar.es](mailto:marrodan@unizar.es)

<sup>2</sup>CNRS-LRGP-Nancy (France)

<sup>3</sup>CNRS-PC2A-Lille (France)

<sup>4</sup>Politecnico di Milano-Milan (Italy)

## Abstract

Biogas (mainly methane and carbon dioxide) produced from biomass anaerobic digestion is considered as a potential renewable gas-phase fuel. That is why the study of the mutual effects of CH<sub>4</sub>/NO<sub>x</sub> have attracted considerable attention in the past decade. In this work, the oxidation of methane with and without NO<sub>x</sub> addition has been investigated in a jet-stirred reactor.

## Introduction

The limited fossil fuel resources and its harmful effects on climate, have increased the interest for environmentally friendly fuels. Biomass seems to be a promising fuel due to its sustainability, security supply and low threat to the environment. Produced from biomass anaerobic digestion, the so-called “biogas”, consists mainly of methane (CH<sub>4</sub>) and carbon dioxide (CO<sub>2</sub>) with trace amounts of nitrogen and sulphur compounds. Biogas can play an important role as potential renewable gas-phase fuel. The main nitrogen compound present in biogas is ammonia, which could easily convert to NO in presence of oxygen. Moreover, exhaust gas recirculation is an effective technique to reduce the pollutants by diluting reactants with exhaust gases working under high dilution and comparatively low temperature conditions. In addition to CO<sub>2</sub> and H<sub>2</sub>O, exhaust gases also contain NO<sub>x</sub> (NO+NO<sub>2</sub>) which, under these conditions, may have a significant impact on ignition characteristics. Despite the abundant experimental reports concerning CH<sub>4</sub>-NO<sub>x</sub> interactions (for example, [1, 2]), the sensitizing effects of NO<sub>2</sub> on methane low-temperature oxidation in a jet-stirred reactor has not been performed yet.

In this context, the aim of the present work is to analyze the CH<sub>4</sub>-NO<sub>x</sub> interactions in a jet-stirred reactor (JSR) at atmospheric pressure, temperatures ranging from 650-1200 K and for different equivalence ratios ( $\phi$ ) with an intense effort in searching important intermediate species, such as HONO, CH<sub>3</sub>NO<sub>2</sub> and HCN.

## Methodology

The experimental setup used to perform the different methane (1%) oxidation experiments, with and without NO<sub>x</sub> addition, was a laboratory-scale spherical fused silica JSR (volumen of 85 cm<sup>3</sup>). A complete description can be found in [3], therefore, only the main features are mentioned here. The reactant gases are premixed and preheated before entering the reactor. The JSR has four injectors with nozzles which create high turbulence and homogenous mixing. The reactor temperature (650-1200 K) is measured by a type-K thermocouple located in the center of the reactor. The pressure inside the reactor is controlled by a needle valve positioned downstream of the reactor and kept at 107 kPa. Different NO and NO<sub>2</sub> concentrations in the reactant mixture have been tested: 0, 100, 500 and 1000 ppm in the case of NO, and 0, 100 and 400 ppm in the case of NO<sub>2</sub>. Argon has been used as bath gas and the residence time inside the reactor was kept constant at a value of 1.5 s. The oxygen required to perform the different oxidation experiments has been varied to work under fuel-lean ( $\phi=0.5$ ) to fuel-rich ( $\phi=2$ ) conditions. Four different diagnostics techniques have been used to analyze the gases leaving the reactor: gas chromatography (GC), chemiluminescence NO<sub>x</sub> analyzer, continuous wave Cavity Ring-Down Spectroscopy (cw-CRDS) and Fourier Transform Infrared spectroscopy (FTIR).

A detailed kinetic mechanism from the POLIMI group [4] has been used to interpret the experimental data. Numerical calculations have been conducted with CHEMKIN-PRO software package. Transient solver has been applied in the simulation tasks with sufficient time to allow reaching the steady state solution.

## Results and conclusions

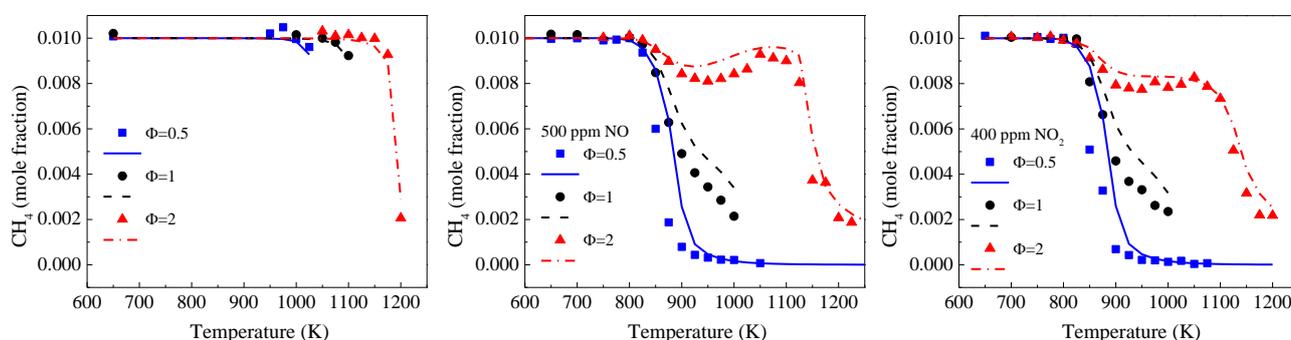
Figure 1 shows the results obtained for  $\text{CH}_4$  consumption in the absence and presence of  $\text{NO}_x$  for the different equivalence ratios analyzed ( $\phi$ ). The results indicate that the onset temperature for methane oxidation (above 1025 K) is shifted to higher temperatures (825 K) by the addition of NO or  $\text{NO}_2$ , independently of the equivalence ratio. This fact indicates that  $\text{CH}_4$  oxidation is promoted by the addition of  $\text{NO}_x$ . The consumption of  $\text{CH}_4$  exhibits a similar trend in the presence of both NO and  $\text{NO}_2$ . New experimental data and new species detection during the low-temperature  $\text{CH}_4$  and  $\text{CH}_4+\text{NO}_x$  jet-stirred reactor oxidation have provided insights into the understanding of the mutual effect of  $\text{CH}_4$  and  $\text{NO}_x$ . The agreement between experimental data and model predictions is very satisfactory. With the help of the kinetic mechanism, reaction rate and sensitivity analysis were performed to identify the main reaction routes and illustrate the kinetic regimes. The analysis of the results indicates that the similar effect on promoting  $\text{CH}_4$  oxidation by either the addition of NO or  $\text{NO}_2$  can be explained because both species are involved in a reaction cycle interchanging them via  $\text{NO}_2+\text{H}/\text{CH}_3=\text{NO}+\text{OH}/\text{CH}_2\text{O}$  and  $\text{NO}+\text{HO}_2/\text{CH}_3\text{O}_2=\text{NO}_2+\text{OH}/\text{CH}_3\text{O}$  reactions. During this reaction sequence highly reactive OH radicals are produced, which promote methane oxidation.

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**Figure 1.** Experimental (symbols) and modeling calculations (lines) for  $\text{CH}_4$  oxidation in the absence of  $\text{NO}_x$  (left), in the presence of 500 ppm of NO (middle) and in the presence of 400 ppm of  $\text{NO}_2$  (right) for the different equivalence ratios ( $\phi$ ) considered.