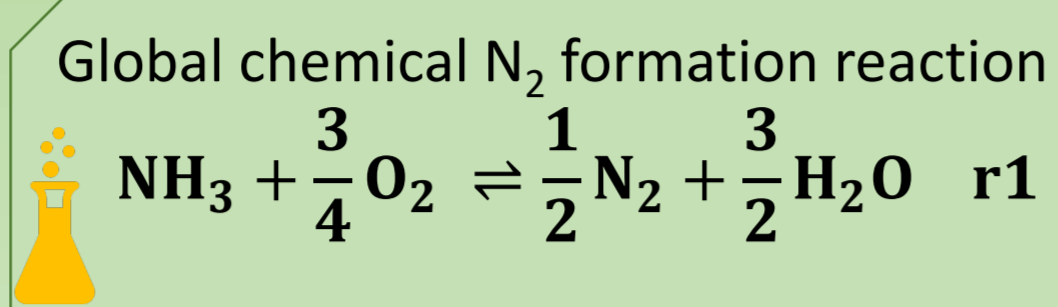


Experimental and Simulated Study of Ammonia Combustion at High Pressures

Pedro García-Ruiz, María Uruén, María Abián, María U. Alzueta
 Thermochemical Process Group (GPT), Department of Chemical and Environmental Engineering
 Aragón Institute of Engineering Research (I3A)
 University of Zaragoza. 50018-Zaragoza, Spain
 p.garcia@unizar.es

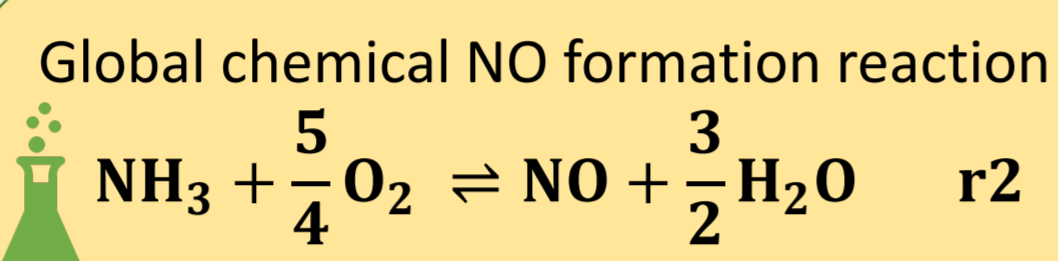
Introduction

Ammonia (NH₃) is an important carbon-free fuel carrier → combustion with no carbon dioxide (CO₂) emissions.



Advantages: It can be burned directly [2] producing water and nitrogen (N₂) and it could be obtained using renewable energy sources and raw materials

Applications: Security of energy supply and storage, transportation and gas turbines [1].

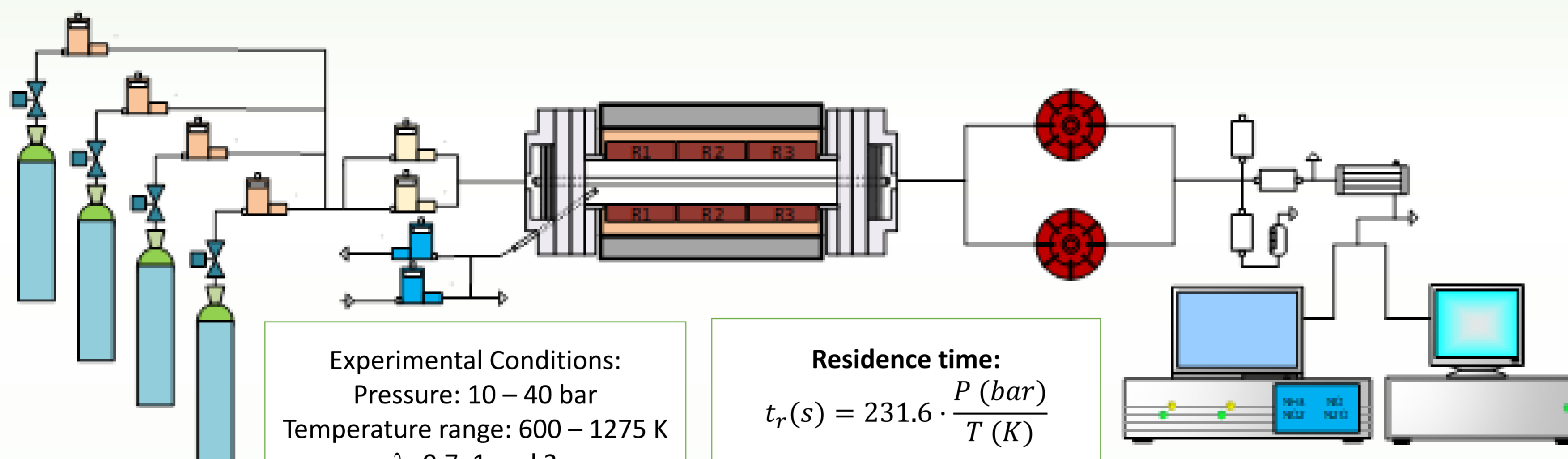


Disadvantages: Obtained from CH₄ and nitrogen oxides (NO_x) can be formed from NH₃ oxidation [3].

Objective:

- Extending the knowledge of oxidation of pure ammonia at high pressure
- Development of a detailed reaction kinetic model

Methodology



Experimental Conditions:
 Pressure: 10 – 40 bar
 Temperature range: 600 – 1275 K
 λ: 0.7, 1 and 3
 [NH₃] = 1000 ppm
 Quartz tubular reactor

Residence time:

$$t_r(s) = 231.6 \cdot \frac{P(\text{bar})}{T(\text{K})}$$

Oxygen excess ratio, Lambda:

$$\lambda = \frac{\left(\frac{\text{NH}_3}{\text{O}_2}\right)_{\text{inlet}}}{\left(\frac{\text{NH}_3}{\text{O}_2}\right)_{\text{stoichiometric}}}$$

Table 1: Matrix of experimental conditions.

Set	NH ₃ (ppm)	O ₂ (ppm)	P (bar)	λ
1	1023	761	10	1,0
2	1019	2143	10	2,9
2R	983	2092	10	2,8
3	1053	745	20	1,0
4	1036	2230	20	3,0
5	1066	778	30	1,0
6	1068	2203	30	2,9
7	982	538	40	0,7
8	1070	765	40	1,0
9	1039	2265	40	3,0

- Chemical kinetic mechanism with **1468 reactions**
- Glarborg et al. development and our research group updates

Experimental Results

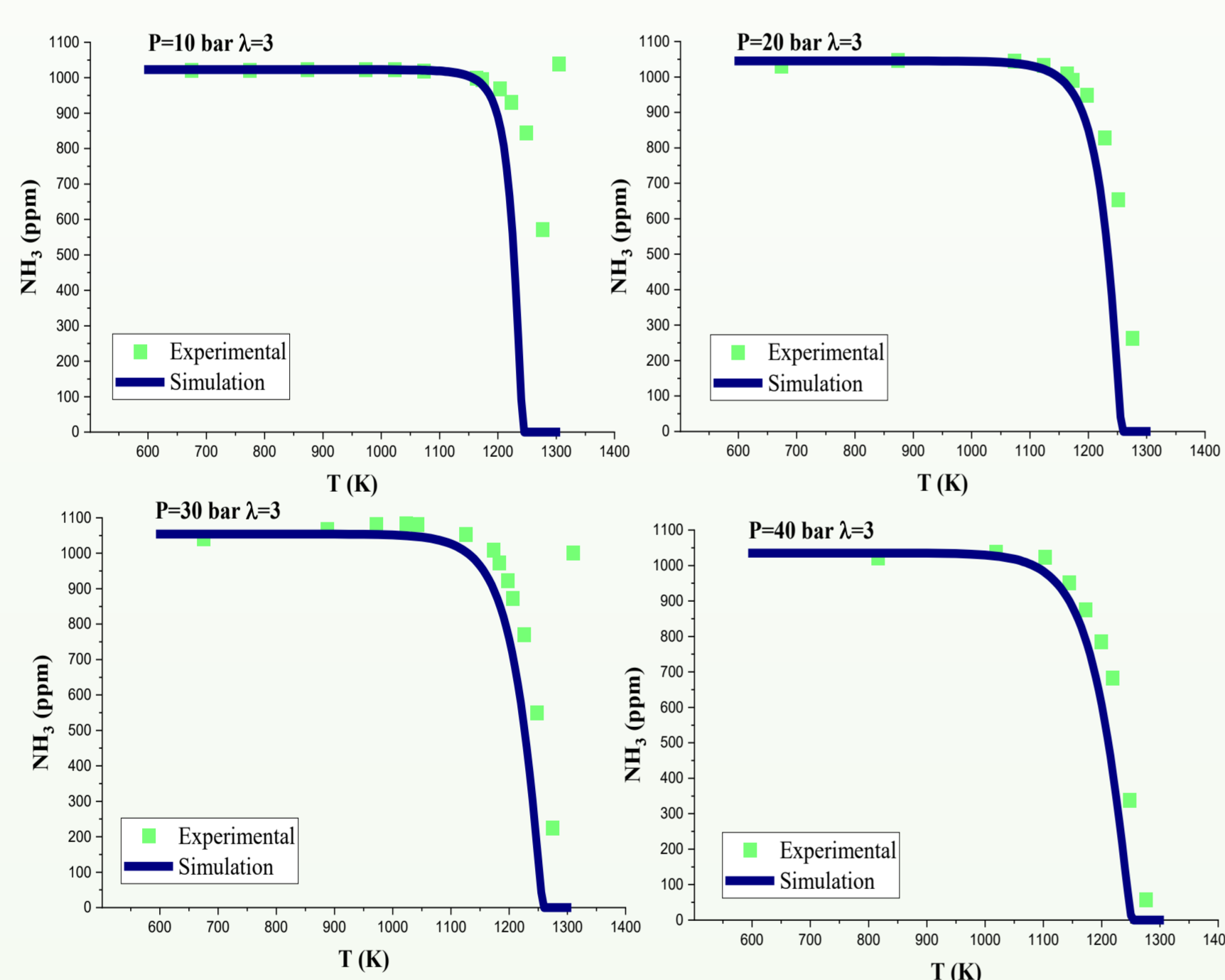


Figure 1: Comparison of experimental and simulated NH₃ concentration at 40, 30, 20 and 10 bar of pressure, λ=3.

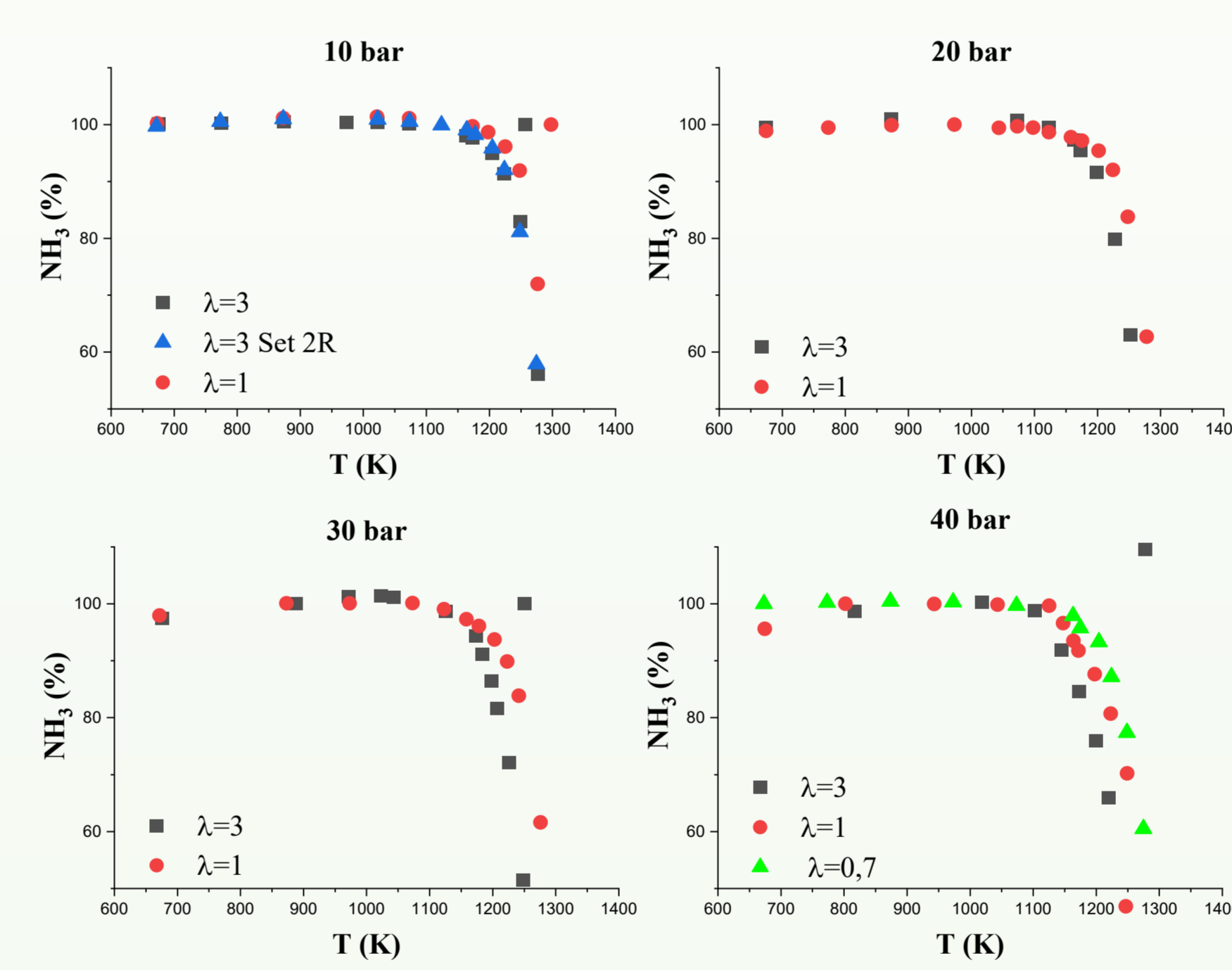


Figure 1: Experimental results of NH₃ concentration (ppm) as a function of temperature, all set of Table 1.

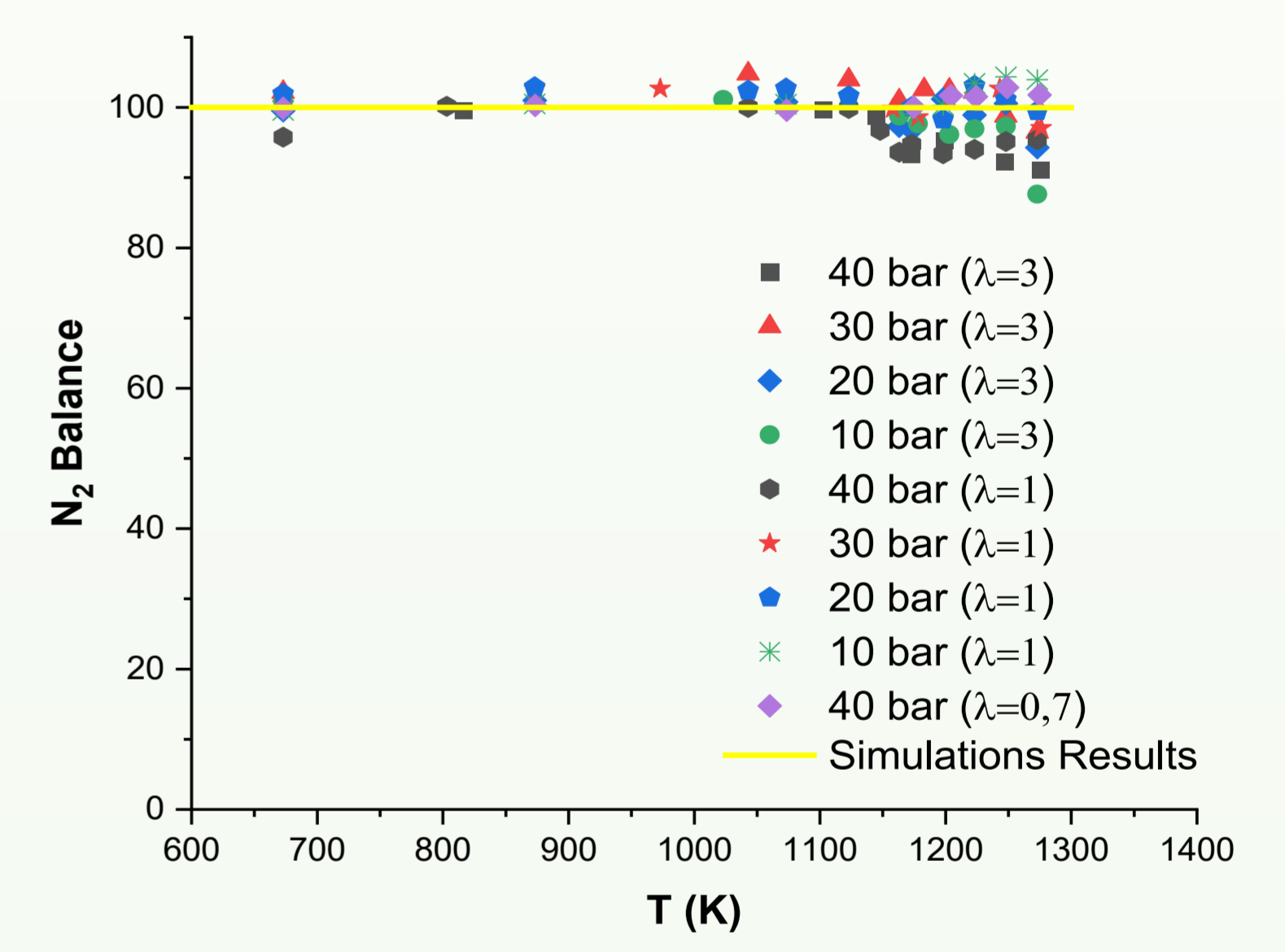


Figure 3: Comparison N₂ balance of experimental and simulated results as a function of the reactor temperature

- λ=3 (Figure 1): ↑ Pressure, ↓NH₃ oxidation onset temperature, 20 – 30 K
- N₂ is the main product of ammonia oxidation, no significant amounts of NO, NO₂, N₂O were produced.
- Modelling predictions show a good agreement with experimental results, full conversion of ammonia is overpredicted to occur at 1250 K approximately.

Conclusions

- ❖ The main nitrogen containing product formed in NH₃ oxidation reaction is N₂, no significant amounts of NO, NO₂, or N₂O were formed.
- ❖ At λ=1 and 3, NH₃ oxidation reaction starts at lower temperatures as the pressure increases.
- ❖ The kinetic model reproduces well the experimental trends obtained, even though simulations slightly overpredict conversion of ammonia.
- ❖ NH₃ conversion is higher at λ=3 than λ=1 at the same conditions of temperature and pressure.

References:

[1]. VALERA-MEDINA, A., XIAO, H., OWEN-JONES, M., DAVID, W. I.F. and BOWEN, P. J. Ammonia for power. *Progress in energy and combustion science*. 2018. Vol. 69, p. 63–102.
 [2]. KOBAYASHI, H. Ammonia Combustion for Energy System. *Japan-Norway Hydrogen Seminar*. 2017.
 [3]. GLARBORG, P., MILLER, J. A., RUSCIC, B. and KLIPPENSTEIN, S. J. Modelling nitrogen chemistry in combustion. *Progress in Energy and Combustion Science*. 2018. Vol. 67, p. 31–68.

Acknowledgements:

The authors acknowledge the funding from the Aragón Government (Ref. T22_17R), co-funded by FEDER 2014-2020 "Construyendo Europa desde Aragón", and to MINECO and FEDER (Project RTI2018-098856-B-I00: Study of the oxidation of NH₃ and its mixtures with CH₄/H₂, evaluating the impact on pollutant) and MINECO PRE2019-090162 for financial support.